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Solution: 37.63 $\frac{m^3}{s} - 32 \frac{m^3}{s} = a$. $a = 5.63 \frac{m^3}{s} = \frac{5.63}{1000} \frac{m^3}{s} = 0.00563 \frac{m^3}{s} = 0.00563 \frac{m^3}{s} \times 1000 \frac{L}{m^3} = 5.63 \frac{L}{s}$ (32 $\frac{m^3}{s} = 32 \frac{m^3}{s} \times 1000 \frac{L}{m^3} = 32000 \frac{L}{s}$) $32000 \frac{L}{s} - 5.63 \frac{L}{s} = 31994.37 \frac{L}{s}$ (53.342) (540 R) (12) $31994.37 \frac{L}{s} \times 0.001 \frac{m^3}{L} = 31.99437 \frac{m^3}{s}$ c. $31.99437 \frac{m^3}{s} = 31.99437 \frac{m^3}{s} \times 1000 \frac{L}{m^3} = 31994.37 \frac{L}{s}$

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Solution: Income = Fixed Costs Variable Costs Dividend = 20% per year 4,000 120,000 3,600 (a) Let N = no. of equipment produced in break-even Income = Total Cost = Fixed Cost = 120,000 + 3,600(N) Income = Total Cost ()

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Solution: $W = -2384.378 \text{ BTU/min}$ $W = 56.235 \text{ hp}$. A thermodynamic steady flow system receives 4.56 kg per min of a fluid where $p_1 = 137.90 \text{ kPa}$, $v_1 = 0.0388 \text{ m}^3/\text{kg}$, $V_1 = 122 \text{ m/s}$, and $u_1 = 17 \text{ kJ/kg}$. The fluid leaves the system at a boundary where $p_2 = 551.6 \text{ kPa}$, $v_2 = 0.193 \text{ m}^3/\text{kg}$, $V_2 = 183 \text{ m/s}$ and $u_2 = 52.80 \text{ kJ/kg}$.

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Given: $U = -316.5 \text{ kJ}$ $k = 1.35 \text{ m} = 2.268 \text{ kg}$ $T_1 = 204.4 + 273 = 477.4 \text{ K}$ $R = 430 \text{ J/kg.K}$ Solution: (a) $W_n = \int p dv$; constant volume $W_n = 0$ (b) $Q = U + W_n = -316.5 + 0 = -316.5 \text{ kJ}$ (c) i. $cv = R/(k-1) = 430/(1.35-1)$ $cv = 1228.57 \text{ J/kg.K} = 1.22857 \text{ kJ/kg.K}$ ii. finding for T_2 $Q = mcv(T_2 - T_1) - 316.5 = (2.268)(1.22857)(T_2 - 477.4)$ $T_2 = 363.81 \text{ K}$ iii.

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